Application No. 10/538,700 Paper Dated: October 30, 2008

In Reply to USPTO Correspondence of May 30, 2008

Attorney Docket No. 5503-051645

AMENDMENTS TO THE CLAIMS

This listing of claims will replace all prior versions, and listings, of claims in the application.

Listing of Claims

1-10. Cancelled.

- 11. (Currently Amended) A method for controlling evaporators in refrigeration plants, which refrigeration plants comprise a refrigerant circuit with a compressor, a liquefier, an expansion valve and an evaporator, wherein the onset of control is carried out—after—the evaporation process—has—begunis controlled, with—whereby—the evaporation pressure at the inlet of the evaporator is measured normally beingand used as one a first_control variable and the refrigerant supercooling temperature upstream of the injection expansion valve is measured and being used as second control variable for the control of the expansion valve, so that in this way the start of evaporation is defined and controlled.
- 12. (Previously Presented) The method for controlling evaporators in refrigeration plants as claimed in claim 11, wherein an internal heat exchanger IHE is connected downstream of the evaporator.
- 13. (Currently Amended) The method for controlling evaporators in refrigeration plants as claimed in claim 11, wherein a further measured value, the temperature of the suction-vapor temperature at the compressor inlet is measured, and said measured value is used to optimizes this control and ensures protection for the compressor.
- 14. (Currently Amended) The method for controlling evaporators in refrigeration plants as claimed in claim 11, wherein further measured values, such as the het-gas-temperature at the exit of the compressor, and/or the compressor oil temperature; and/or the suction-pressure at the compressor inlet and/or the high-pressure upstream of the injection-expansion valve or downstream of the compressor are measured, and said measured values ear beare used to optimize or protect the compressor.

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15. (Currently Amended) The method for controlling evaporators in refrigeration plants as claimed in claim 11, wherein a refrigerant is used with a predetermined phase-boundary curve in an lg (p, h) diagram, said phase-boundary curve having a left-hand rising part, a maximum and a right-hand falling part, and control is effected, optimally for the particular type of evaporator, such that the start of the evaporation begins near to the left-hand limit-part of said boundary-phase curve of the lg p, h diagram for said refrigerant.

- 16. (Currently Amended) The method for controlling evaporators in refrigeration plants as claimed in claim 11, wherein this type of control causes the evaporator to be flooded and the degree of flooding to be determined, and wherein the temperatures of the refrigerant suction vapor at the compressor inlet and of the refrigerant liquid are measured and at the same time eauses the refrigerant suction vapor temperature and refrigerant liquid temperature to be are monitored and controlled.
- 17. (Currently Amended) The method for controlling evaporators in refrigeration plants as claimed in claim 11, wherein a temperature or pressure value of the refrigerant is measured within the circuit for limiting the vapor temperature upstream of the compressor, and thesaid measured value for limiting the suction-vapor temperature upstream of the compressor over-controls the evaporation control and keeps the suction-vapor temperature constant at an optimum and/or maximum value as a function of the compressor.
- 18. (Currently Amended) The method for controlling evaporators in refrigeration plants as claimed in claim—1+12, wherein a refrigerant is used with a predetermined phase-boundary curve in an lg (p, h) diagram, said phase-boundary curve having a left-hand rising part, a maximum and a right-hand falling part, and wherein the optimum of the process is always in favor of the evaporator and not the IHE to achieve maximum utilization of the enthalpy in the evaporator between the left-hand and right-hand parts of the phase-boundary limit-curves of the lg (p, h) diagram for said_refrigerant and, depending on the temperature level of the IHE, with a superheating component in the evaporator.

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19. (Currently Amended) The method for controlling evaporators in refrigeration plants as claimed in claim 1+12, wherein one evaporator can be connected to one IHE, or a plurality of evaporators can be connected to one IHE or a plurality of evaporators can be connected to a plurality of IHEs, or any type of combinations thereof, to form a refrigeration system.

20. (Currently Amended) The method for controlling evaporators in refrigeration plants as claimed in claim 12, wherein, depending on the combination of evaporators, IHEs, injectionexpansion valves and compressors, each injection valve and the system can be controlled with reduced measured values.

21. (Currently Amended) The method for controlling evaporators in refrigeration plants as claimed in claim ++17, wherein the measured value for limiting the corresponding alternative measured valveyapor temperature upstream of the compressor over-controls the evaporation control and keeps the suetion-vapor temperature upstream of the compressor constant at an optimum and/or maximum value as a function of the compressor.

22. (Previously Presented) The method for controlling evaporators in refrigeration plants as claimed in claim 20, wherein one measured value is controlled for each expansion valve.

23. (Previously Presented) The method for controlling evaporators in refrigeration plants as claimed in claim 20, wherein one measured value is controlled for each compressor.

24. (Previously Presented) The method for controlling evaporators in refrigeration plants as claimed in claim 20, wherein one measured value is controlled for a plurality of expansion valves.

25. (Previously Presented) The method for controlling evaporators in refrigeration plants as claimed in claim 20, wherein one measured value is controlled for a

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plurality of compressors.

26. (Currently Amended) The method for controlling evaporators in refrigeration plants as claimed in claim 11, wherein depending on the combination of evaporators, IHEs, injectionexpansion valves and compressors, each injection-expansion valve and the system can be controlled with a combination of one or more measured values.